

Study on the erosion wear in pipe fittings

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ABSTRACT

In the pipeline system for slurry, local erosion wear failure has become the main damage mechanism of pipe in the fracturing operations of oil-gas engineering. Computational Fluid Dynamics simulation is performed to determine the evolutionary process of erosion wear in tubing connector, which is the resistance of pipeline system, and a new way to predict the pipeline longevity is provided. Based on the Euler equation, solid particle concentration in the slurry and interphase momentum exchange are included in the liquid flow equations due to the influence of dense particle on slurry (slurry is a two-phase flow), and the particle trajectory were calculated in the Lagrange frame by analyzing the forces from the interaction of liquid and particle and particles impact. With the erosion damage model, the erosion rate/depth in the connector was calculated to reconstruct the mesh model of shoulder with 5 tori. Torus 1 is closest to axis while torus 5 is on the outmost wall of the connector. During the erosion event, greatest erosion and hence surface deformation occurs on tori 1 and 2, and this affects the surrounding

flow and particle movement. After 10 hours of erosion, there was a dramatic drop in the maximum erosion rate, which illustrated a conservative prediction for pipeline service life if the initial erosion rate was used. An erosion experimental setup was also performed to identify the weight loss and erosion characteristic of the inner surface with erosion time of 55 hours. It was observed that the erosion simulations provided relative errors within 18% for erosion length and weight loss compared to the experimental values and a closed form equation for the erosion rate was proposed to predict the erosion life of tubing connector.

Keywords: slurry erosion; impact; steel; erosion testing; numerical simulation.

Nomenclature

μ liquid viscosity

K consistency coefficient

n flow index

$\dot{\gamma}^{n-1}$ shear rate

α_q fluid volume fraction in a control volume

ρ liquid density

t time

$u_i (u_j)$ i (j) direction velocities of fluid

p liquid static pressure

$-\rho u'_i u'_j$ stress tensor

m_p the particle mass

F_{si} external body forces arisen from interaction with the particles

δV volume of control volume

F_{drag} drag force per unit particle mass

ρ_p particle density

d_p particle diameter

C_D drag coefficient

Re relative Reynolds number

F_{pressure} force arisen from the pressure gradient of fluid

$F_{\text{virtual_mass}}$ force required to accelerate the fluid surrounding the particle

C_{vm} virtual mass factor

u_p particle velocity

$F_{\text{collision}}$ forces arisen from the particle collision

e_{ij} unit vector defined from particle i to particle j

$x_{pi}(x_{pj})$ position of particle $i(j)$

k spring constant k

u_{pr} relative velocity between two colliding particles

\mathcal{E}_d fraction of the diameter for allowable overlap

E_r erosion rate in $\mu\text{m}/\text{kg}$ (total particle feed)

K a material constant with a value of 2.0×10^{-9} for steel

ρ_w steel density

A area of sub-area impacted by particle

M total number of particles fed

n_{hit} number of particle impacting the sub-area

m particle velocity exponent

α impingement angle

x_i^k i direction coordinate at time t_k ,

x_i^0 original coordinate

e_i unit i direction location vector

n_i^j unit outward normal vector of small area at time t_j

dx_i^j erosion deformation at the j time period $[t_{j-1}, t_j]$

E_{rj} erosion rate at time t_j

INTRODUCTION

Erosion wear is a common phenomenon of slurry flow in pipe, which can remove material from the wall due to the impact of particles, and the thickness reduction caused by erosion is an important consideration in design and safety evaluation of pipe. The method to test the weight loss of the pipe has been widely used to identify the erosion level (Finnie, 1960; Tilly, 1979), but the evolution of erosion characters in the inner surface cannot be obtained through the test. Nowadays, the numerical simulation method for particle movement has been realized by combining multiphase flow model with erosion model to predict the wall erosion for the pipe fittings (such as bend and connector) (Huser et al., 1998; Ping et al., 2017; Guofu et al., 2018), and detailed information about erosion position and erosion rate could be obtained (Mazumder et al., 2005; Joseph et al., 2009). Chong et al. (2013) employed Computational Fluid Dynamics (CFD) method to simulate the flow field and the erosion characteristics on the surface of annular with the Euler-Lagrange method (Badr et al., 2005; Davis et al., 2009) based on the fixed mesh model. Combined with the overall erosion distribution features on surfaces, the erosion rate was predicted, but it was significantly over-predicted up to 100% of experimental values by the 38 μm - sized particles on the forward-facing step. Because the wear deformation of the inner wall is ignored during the simulation progress, the method mentioned above is only available for the initial stage of erosion, which has a negligible effect on the flow field (Man-Lai et al., 2011). Obviously, the erosion wear on the inner wall is accumulated to affect the flow in pipe eventually, and interaction of flow and wall deformation should be considered for determining the evolutionary process of erosion wear, according to which the erosion life of pipe can be precisely attained. The purpose of the current work was to predict the erosion wear of the tubing connector by using mesh reconstruction technique to simulate the erosion deformation on wall, and the obtained simulation result was compared with the experimental data.

METHODS

2.1 EXPERIMENT

In order to investigate the erosion of a horizontal pipe by silica sand (Figure 1), an experimental rig was built (Figure 2). The fracturing fluid, which is used for fracturing in oil and gas fields, is pumped into a horizontal pipe by piston pump, forming a loop through the high pressure pipe. The flow is controlled by electric control valve and measured by flowmeter. The pressure drop of tubing is determined by measuring the inlet and outlet pressure of tubing with pressure gauge. To avoid the slurry settlement during experiments, the fracturing fluid must be continuously stirred in the agitator tank.

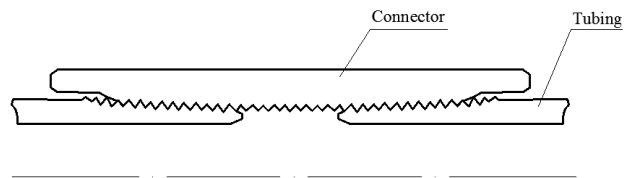


Figure 1. The structure of tubing connector

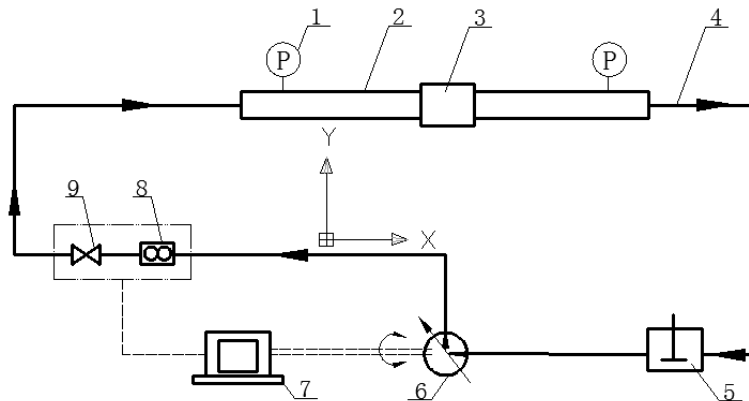


Figure 2. Schematic diagram of experimental rig for tubing connector

- 1 - Pressure gauge; 2 - Tubing; 3 - Connector; 4 - High pressure pipe; 5 - Agitator tank;
6 - Piston pump; 7 - Control system; 8 - Flowmeter; 9 - Electric control valve

By using screen mesh, the grain size of silica is filtered to 150 μm , and the particle volume

fraction is 26%. As the infusion is non-Newtonian fluid, viscosity varies with rotational speed and is measured by a torque rheometer, revealing that the rheological behavior of fracturing fluid obeys the Non-Newtonian power law properly, and it is described as (Mitsoulis, 2007)

$$\mu = K\dot{\gamma}^{n-1} \quad (1)$$

When the experimental temperature is 35°C, n is 0.651, and K is 29.01 mPa.sⁿ. Considering the temperature rise caused by circulating flow in the experimental pipeline, the liquid temperature is monitored, in case experimental temperature deviated greatly from the reference value (35°C). Once the temperature reaches 38°C, the pump stops running. When the total time of several erosion experiences reaches the setting, the weight loss of connector is measured with electronic scale, and the connector is slit to show the erosion characteristic.

2.2 NUMERICAL SIMULATION

2.2.1 THE FLUID FLOW MODEL

The complete model for the erosion wear consists of the fluid flow equations, the particle motion equation and erosion damage model. When the particle volume fraction is low (<10%), the Discrete phase model (DPM) (Noon et al., 2016) is appropriate to describe the dilute particle flow because the influence of particle on liquid flow can be ignored. However, solid particle concentration in the fracturing fluid is high enough to affect the liquid flow, so the flow equations should be modified by including the item related with the particle volume fraction and interphase momentum exchange. It is described as (Hager et al., 2018)

$$\frac{\partial(\alpha_q \rho)}{\partial t} + \frac{\partial(\alpha_q \rho u_j)}{\partial x_j} = 0 \quad (2)$$

$$\begin{aligned} \frac{\partial}{\partial t}(\alpha_q \rho u_i) + \frac{\partial}{\partial x_j}(\alpha_q \rho u_i u_j) = & -\alpha_q \frac{\partial p}{\partial x_i} + \alpha_q \rho g_i + \frac{\partial}{\partial x_j}(\alpha_q \mu \frac{\partial u_i}{\partial x_j}) - \frac{\partial}{\partial x_j}(\alpha_q \rho u_i' u_j') \\ & + \frac{F_{si} \cdot m_p}{\delta V} \end{aligned} \quad (3)$$

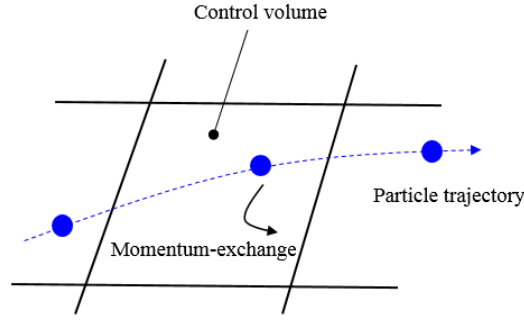


Figure 3. Momentum transfer between fluid and particle

As shown in Figure 3, the momentum transfer from the fluid to the particle is determined by examining the change in momentum of a particle as it passes through each control volume. This momentum change equals the external force, and is described by (Noon et al., 2016)

$$F_{si} = \sum (F_{drag} + F_{pressure} + F_{virtual_mass}) \quad (4)$$

Where F_{drag} is computed as follows (Haider et al., 1989):

$$F_{drag} = \frac{3\mu C_D Re}{4\rho_p d_p^2} (u_i - u_{pi}) \quad (5)$$

Re can be written as (Mitsoulis, 2007):

$$Re = \frac{\rho_p d_p |u_{pi} - u_i|}{\mu} \quad (6)$$

$F_{pressure}$ is computed as follows (Cundall et al., 1979):

$$F_{pressure} = \frac{\rho}{\rho_p} u_p \frac{\partial u_j}{\partial x_j} \quad (7)$$

$F_{virtual_mass}$ is described as (Cundall et al., 1979):

$$F_{virtual_mass} = C_{vm} \frac{\rho}{\rho_p} (u_p \frac{\partial u_j}{\partial x_j} - \frac{du_p}{dt}) \quad (8)$$

Additionally, when the flow is turbulent, the k-ε model is used for turbulence modeling.

2.2.2 THE PARTICLE MOTION EQUATION AND EROSION DAMAGE MODEL

Particle motion is determined by solving the particle motion equation in Lagrange frame

(Hager et al., 2018),

$$\frac{du_p}{dt} = -F_{si} + \frac{g_x(\rho_p - \rho)}{\rho_p} + \sum_{i=1}^n F_{\text{collisioni}} \quad (9)$$

Where $\sum_{i=1}^n F_{\text{collisioni}}$ is determined by the deformation, which is measured as the overlap between pairs of particles.

e_{ij} is expressed as (Hager et al., 2018):

$$e_{ij} = (x_{pi} - x_{pj}) / \|x_{pi} - x_{pj}\| \quad (10)$$

The overlap δ_{ij} (which is less than zero during contact) is defined as follows (Hager et al., 2018),

$$\delta_{ij} = \|x_{pi} - x_{pj}\| - (d_{pi} + d_{pj}) \quad (11)$$

Following the spring collision law of the discrete element method (DEM), the force on particle is computed as follows (Hager et al., 2018):

$$F_{\text{collisioni}} = k\delta_{ij}e_{ij} \quad (12)$$

Here, the value of k can be estimated with the following equation (Hager et al., 2018),

$$k = d_p \rho_p \frac{\pi u_{pr}^2}{3\epsilon_d^2} \quad (13)$$

Equation 9 is integrated in a time step of $\pi\sqrt{m_p/k}$ to capture the trajectory of a particle.

When the particle repeatedly impacts the wall and exceeds the shear strength of steel, a cut is formed on the surface (Wong, 2013). Erosion rate model for a sub-area is given as follow (Bitter 1963; Haugen et al 1995),

$$E_r = \frac{10^6 K}{\rho_w AM} \sum_{i=1}^{nhit} u_i^m F(\alpha_i) \quad (14)$$

Here the erosion rate E_r is erosion depth due to impact of 1 kg particle on this microplane. Haugen et al. (1995) have done the test for determining the material related parameters and $F(\alpha)$ relation

depending on impingement angle (seen Table 1 and Figure 4).

Table 1 Material-dependent parameters for steel grade

Material	K	n	ρ_w
Steel grade	2.0×10^{-9}	2.6	7800 kg/m ³

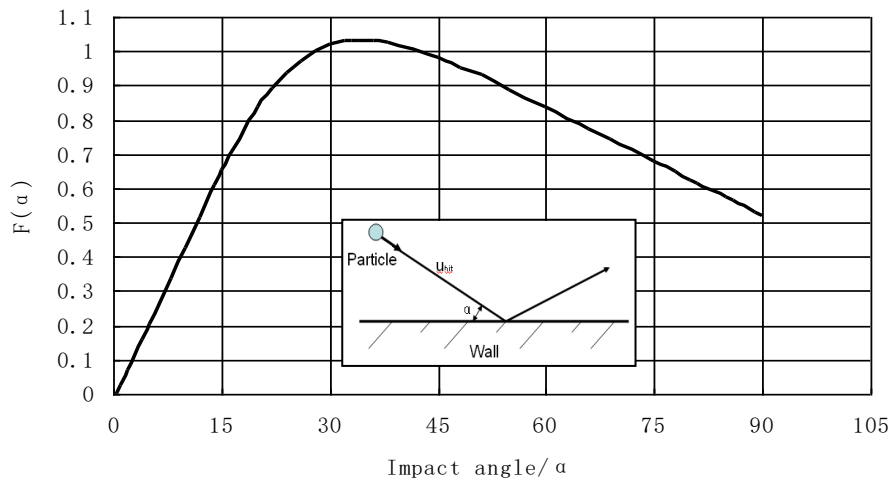


Figure 4. $F(\alpha)$ functional relationship (Haugen et al. 1995)

2.2.3 THE CALCULATION METHOD AND PROCESS

For the unsteady flow simulation, the finite volume method (FVM) and PISO algorithms (Wong et al. 2013) are adopted to derive and solve the discrete equations of fluid flow on a staggered grid.

The fluid-particle coupling simulation is described as follows:

- (1) Calculate the fluid flow equations until a converged solution is achieved in one time step, then uniformly launch N number of particles from the inlet surface ($N=2000$).
- (2) Solve the particle motion equation to get velocity and position of each particle, and then calculate Equation 14 to identify the erosion depth in each wall mesh face.
- (3) Repeat steps (1) ~ (2) until the number of total particles escaping through the outlet is equal to M ($M=234000$).

(4) Calculate Equation 14 to identify the erosion rate and erosion depth for a given time period $[0, t_1]$, and reconstruct the mesh model for next simulation period $[t_1, t_2]$.

(5) Repeat steps (1) ~ (4) to obtain the erosion rate and erosion depth at successive time point t_3, \dots, t_n .

During the process of mesh reconstruction, new location of center is updated according to

$$x_i^k = x_i^0 + \sum_{j=1}^{k-1} dx_i^j (e^j \cdot n_i^j)$$

Here $dx_i^j = E_{rj} \cdot (t_j - t_{j-1})$

RESULTS AND DISCUSSION

The liquid-solid flow model and erosion model were combined to simulate the flow field and erosion rate in a tubing connector. The connector with a horizontal inlet and horizontal outlet is shown in Figure 5. Some assumptions made for simulation, including the fracturing fluid is incompressible and the particles are round and uniform in size. Table 2 shows the relevant parameters.

Table 2 Relevant flow parameters

Description	Condition
Inlet liquid flow velocity	20 m/s
Outlet pressure	0 Pa
Fracturing fluid density	1200 kg/m ³
Tubing inner diameter	45.34 mm
Tubing outer diameter	60.32 mm
Model length	1200 mm
Particle diameter	150 μm

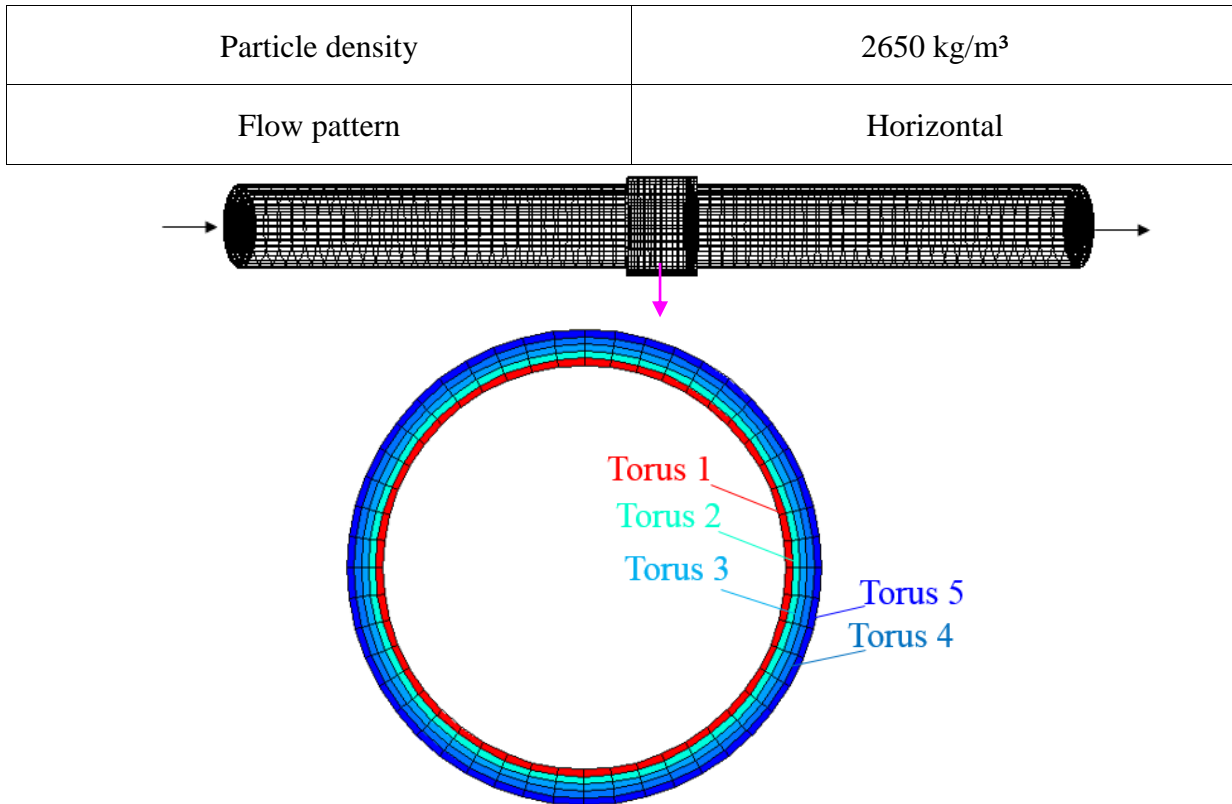


Figure 5. CFD mesh model (33880 hexahedral element)

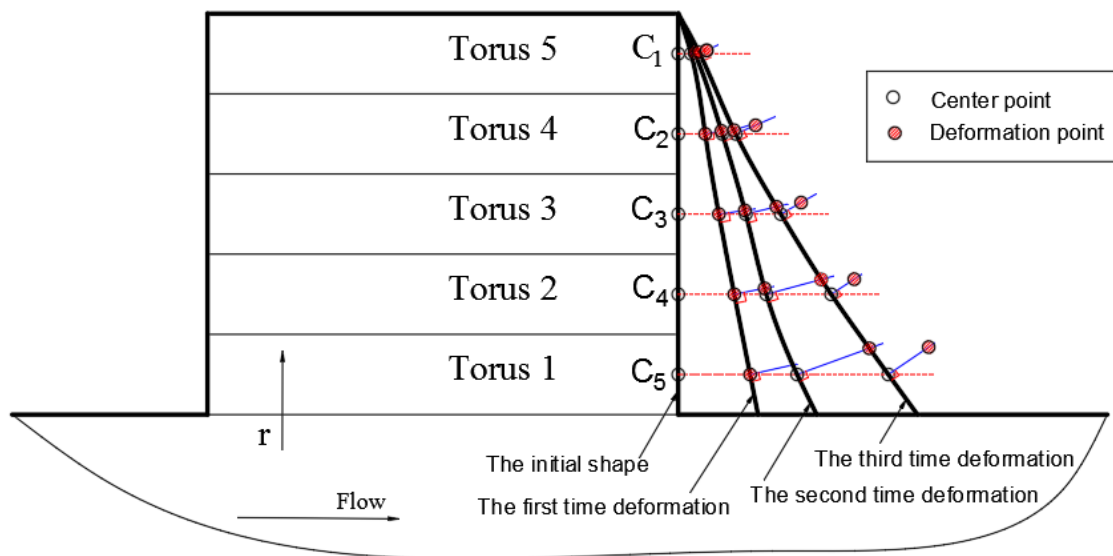
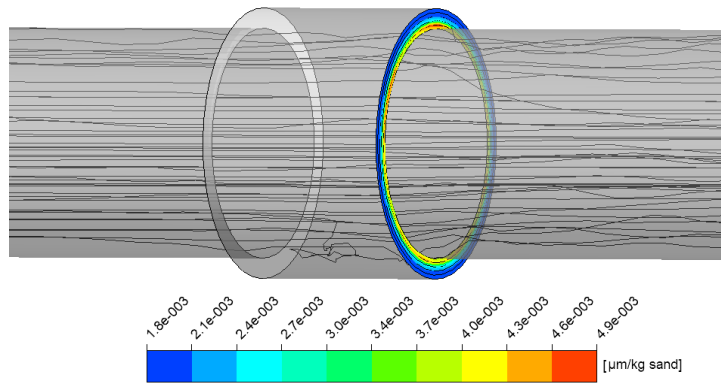


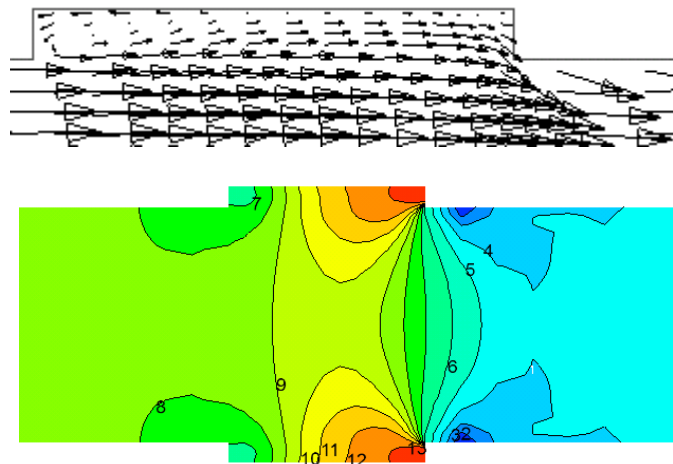
Figure 6 Schematic diagram of new shoulder generatrix for model reconstruction

For the convenience of simulation, the axial symmetry of structure is considered and the shoulder surface, which has the most serious erosion zone, is evenly divided into five tori as shown in Figure 5, and the center points in each torus was marked with $C_1 \sim C_5$ (Figure 6),. After

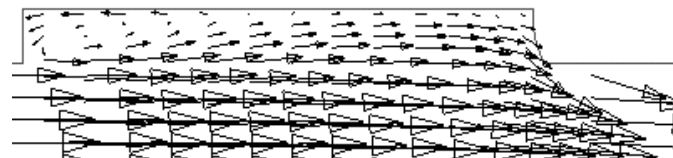
calculating the erosion rates of mesh faces, the erosion depths of center points ($C_1 \sim C_5$) are identified following the erosion rates of area-weighted average for each torus, and the deformation points were respectively located by moving the center points along the normal direction of each torus with the erosion depth. Then the new shoulder generatrix after an erosion time period is formed by connecting deformation points with Bézier curve.



(a)



(b)



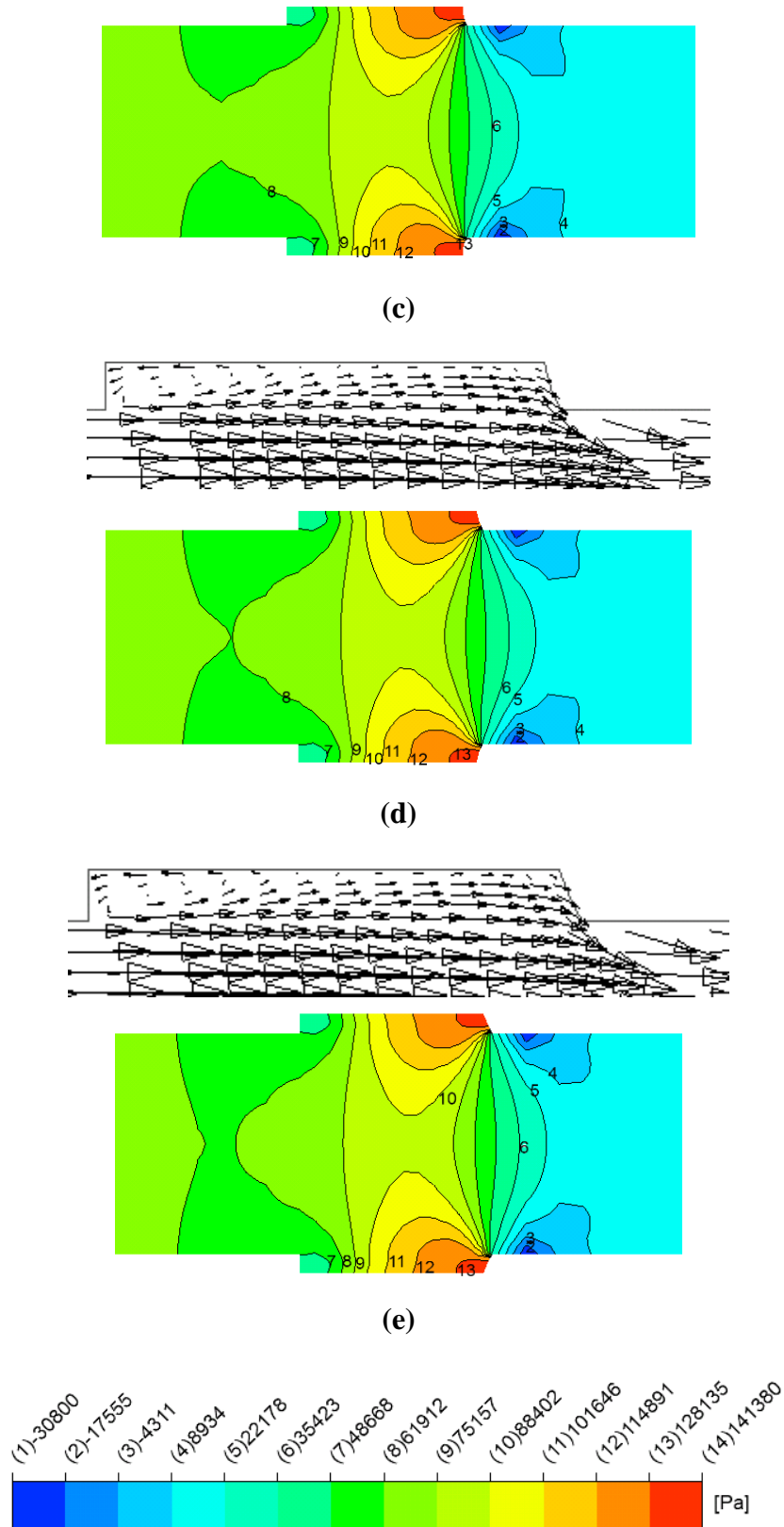


Figure 7 Erosion deformation and flow field at different time (a) particle trajectory and erosion rate contours without erosion deformation; (b) flow field without erosion deformation; (c) flow

field with erosion (15 h); (d) flow field with erosion (35 h); and (e) flow field with erosion (55 h)

Figure 7 shows the particle trajectory and flow field with the erosion wear at the connector. As particle impacts the right shoulder, its trajectory is bended and extend to the straight pipe (Fig. 7a). Obviously, the erosion on the right side of the connector is much more severe than that of the left side. Fig. 7b shows the flow field without erosion deformation. As for connector, the velocity of the fluid flow near the wall is small, meanwhile the backflow appears on the left shoulder, while the velocity increases on the right shoulder. The maximum pressure on the wall is 141380 Pa. During the process of erosion, the right shoulder surface of the connector changes from vertical plane to oblique surface with respect to flow direction (Fig. 7c~7e), indicating that the shape of the right shoulder surface was streamlined by the continuous impact of particles. With the streamlined shoulder, the pressure at the connector junction decreases and the zone of highest pressure contracts away from the center of pipe. Simultaneously, the upstream pressure declines with the isobaric line 14 extending to the pipe center, and the pressure marked with 10 tends to rise.

Figure 8 shows the erosion deformations of the right shoulder surface at different times. Torus 1 has the maximum erosion deformation and decreases progressively to torus 5. When the connector has been eroded for 5h, the torus 1 becomes more streamlined, and the torus 2 is in severe erosion state and is slightly deformed. At the 15th hour of erosion, the shape of torus 2 has changed to be streamlined with an inflection point between torus 1 and torus 2. This makes the torus 1 to be the serious erosion target again. When time exceeds 35h, the total surface of right shoulder streamlined, and the erosion deformation changes more slightly. Therefore, it is interesting to note that the slurry has a greater destructive effect on the connector in the early stages of erosion, and the structure is reshaped into a streamlined shape as the result of the cumulative erosion over a long time.

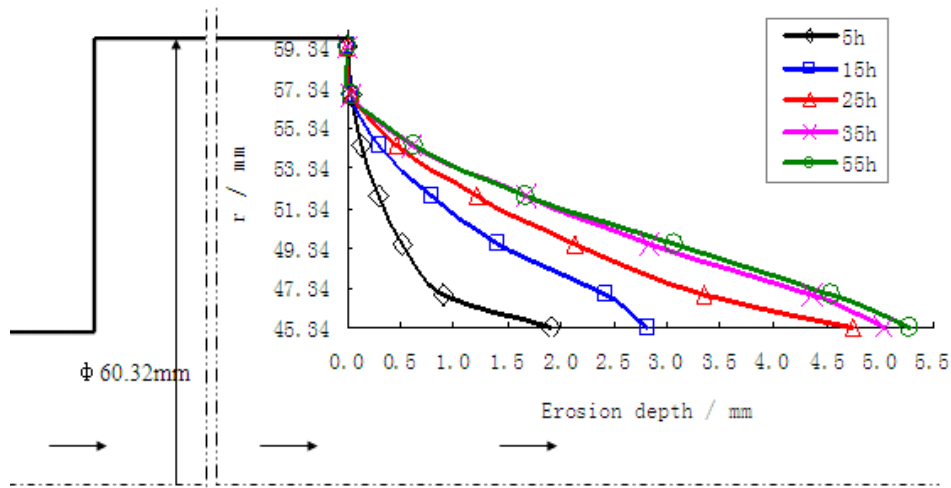


Figure 8 Erosion deformation of right shoulder surface at different time

Figure 9 shows the variation of the average erosion rate of each torus with time. The torus that is close to the center of the pipe has the higher erosion rate. The erosion rate of torus 1 is $4.07 \times 10^{-3} \mu\text{m/kg sand}$ at the beginning, then when the sharp corner at junction is eroded and tends to streamline, the impact strength of particles is weakened, which makes the erosion rate decreases sharply. As the right shoulder surface becomes more and more streamlined, the erosion rate tends to be stable. Furthermore, due to the continuous destruction shape of Torus 1, the flow field and particle trajectory change accordingly, resulting in fluctuation of erosion rate in a certain extent.

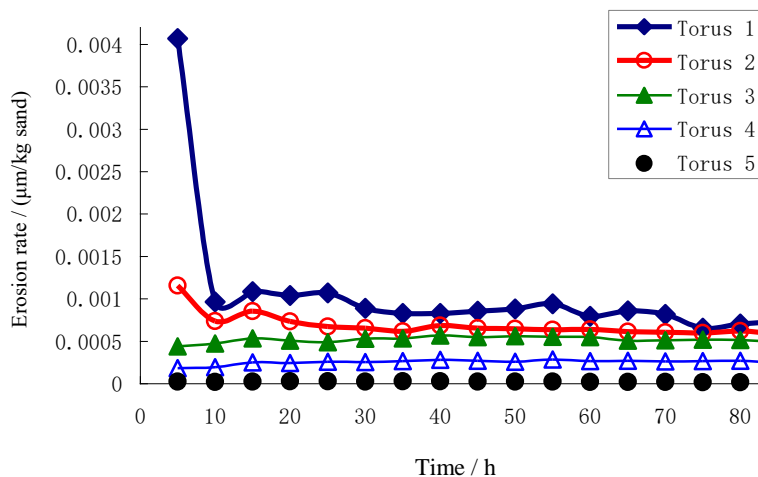


Figure 9 Average erosion rates of five tori



Figure 10 Axial erosion length test (erosion time is 55 h)

Figure 10 shows the erosion of connector. It is more like the axial oblique cutting traces at the right shoulder. After 55 hours of erosion, the experimental axial erosion length and weight loss is 6.2 mm and 0.243 kg respectively, while the predicted results are 5.25 mm and 0.20 kg. The corresponding relative errors are 15.3% and 17.7% respectively, which preliminarily verifies the reliability of the simulation method. Obviously, if the erosion deformation is not considered, the calculated erosion length and weight loss are much higher.

CONCLUSIONS

In summary, we have used numerical techniques and erosion model to predict the erosion wear in the tubing connector. In the simulation, several important interactions of liquid-particle, particle-particle, and fluid-structure were considered and the mesh model of connector was reconstructed according to the wall erosion deformation.

The particle trajectory and the transient erosion deformation, which still cannot be approached through the test, were obtained through the simulation and the peak average erosion rate was found to occur on the inner wall of junction. It was found that the connector shoulder surface extends to be streamlined when the erosion was significant for large amount of sand feed, and the peak erosion rate decreases dramatically from the $4.07 \times 10^{-3} \mu\text{m}/\text{kg sand}$. After 55 hours of erosion,

the maximal erosion length and the weight loss from simulation are equal to 5.25 mm and 0.20 kg, respectively, which show basic agreement with the experiment results.

The study shows the method of transient simulation for the erosion wear, and helps to improve the prediction of the erosion safety for connector in service.

ACKNOWLEDGMENT

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